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# Production of bioadditives from glycerol esterification over zirconia supported heteropolyacids



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## HIGHLIGHTS

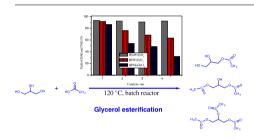
- ► H<sub>4</sub>SiW<sub>12</sub>O<sub>40</sub>/ZrO<sub>2</sub> is an effective catalyst for glycerol esterification.
- A 93.6% combined selectivity of glyceryl diacetate and triacetate is achieved.
- ► H<sub>4</sub>SiW<sub>12</sub>O<sub>40</sub>/ZrO<sub>2</sub> can be reused up to four consecutive runs without deactivation.
- ► H<sub>4</sub>SiW<sub>12</sub>O<sub>40</sub>/ZrO<sub>2</sub> can be resistant to the impurities present in bulk glycerol.

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### ABSTRACT

The synthesis of bioadditives for biofuels from glycerol esterification with acetic acid was performed over zirconia supported heteropolyacids catalysts using  $H_4SiW_{12}O_{40}$  (HSiW),  $H_3PW_{12}O_{40}$  (HPW) and  $H_3PMo_{12}O_{40}$  (HPMo) as active compounds. The as-prepared catalysts were characterized by  $N_2$ -physisorption, XRD, Raman spectroscopy,  $NH_3$ -TPD, FTIR of pyridine adsorption and  $H_2O$ -TPD. Among the catalysts tested,  $HSiW/ZrO_2$  achieved the best catalytic performance owing to the better combination of surface Brønsted acid sites and hydrothermal stability. A 93.6% combined selectivity of glyceryl diacetate and glyceryl triacetate with complete glycerol conversion was obtained at  $120\,^{\circ}C$  and 4 h of reaction time in the presence of  $HSiW/ZrO_2$ . This catalyst also presented consistent activity for four consecutive reaction cycles, while  $HPW/ZrO_2$  and  $HPMo/ZrO_2$  exhibited distinct deactivation after reusability tests. In addition,  $HSiW/ZrO_2$  can be resistant to the impurities present in bulk glycerol.

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## 1. Introduction

As the petroleum reserves deplete and concerns about environmental issues increase, the preparation of biofuels from biomass is stimulating growing interest (Chheda et al., 2007; Juan et al., 2011). In this context, biodiesel has gained considerable attention as a non-toxic, biodegradable and renewable alternative to petroleum-derived fuels. Biodiesel is usually manufactured by

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transesterification of plant and animal oils with methanol or ethanol, with glycerol as a co-product (Juan et al., 2011). With the rapid pace of biodiesel development and commercialization, glycerol is currently produced in a huge amount, which makes the price of glycerol decline sharply. Consequently, it is highly desirable to convert low-cost glycerol into value-added chemicals or materials. In addition, the biomass-derivate glycerol is a nontoxic, edible, and biodegradable compound containing highly multifunctional structure, making it as a versatile building block for the synthesis of a broad family of valuable derivatives by several catalytic processes involving oxidation (Hu et al., 2010; Tsuji et al., 2011), hydrogenolysis (Zhu et al., 2012a,b; Xia et al., 2012; Yuan et al., 2010), dehydration (Tsukuda et al., 2007),

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